

REPLACEMENT CLAIMS

AB 1. (Amended) A process for reducing content of sulphur compounds and polyaromatic hydrocarbons in a hydrocarbon feed stock having a boiling range between 200°C and 600°C, which process comprises the steps of:

(a) contacting the feed stock with hydrogen over a hydrotreating catalyst in a hydrotreating zone at conditions being effective for hydrotreating and obtaining a hydrotreated effluent comprising hydrotreated feed stock, hydrogen sulphide and hydrogen;

A2 (b) cooling the hydrotreated effluent; and

(c) contacting the hydrotreated effluent with a hydrotreating catalyst at conditions being effective for conversion of polyaromatic hydrocarbons to monoaromatic compounds.

A3 4. (Amended) A process of claim 1, wherein step (c) is performed in a final catalyst bed of the hydrotreating zone.

A4 6. (Amended) A process of claim 1, wherein the hydrotreating catalyst used in step (c) is a composite of Group VI-B and/or Group VIII metal on a porous refractory inorganic oxide.

REPLACEMENT PARAGRAPHS

On page 9, lines 19-23:

Table 1

Properties of feedstock used in the following Examples:

Properties	Feedstock A	Feedstock B
SG 60/60	0.9279	0.9924
S (wt %)	1.34	3.53
N (wt ppm)	2677	3594
Aromatics (wt%)		
Mono-	17.7	8.36
Di-	9.9	7.29
Tri-	11.4	36.5

On page 10, lines 1-5:

Table 2

Properties of products in Example 1:

At

Properties	Product A	Product B
SG 60/60	0.8920	0.9411
S (wt %)	0.02	0.1905
N (wt ppm)	526	2046
Aromatics (wt%)		
Mono-	31.0	22.6
Di-	7.8	11.3
Tri-	6.7	23.9
Distillation, D2887 (°C)		
5	236	287
10	267	314
30	342	360
50	392	392
70	437	428
90	495	479
95	518	503

On page 11, lines 3-10:

Table 3

Properties of products in Example 2:

Am

Tem- perature (°C)	LHSV (h ⁻¹)	SG 60/60	S (wt%)	N (wt ppm)	Di- aromatics (wt%)	Tri- aromatics (wt%)	PAH (wt%)
325	6	0.8914	0.0038	505	4.6	5.0	9.6
350	6	0.8911	0.0029	468	4.9	4.9	9.5

On page 12, lines 1-5:

Table 4

Properties of products in Example 3:

AS

Tem- perature (°C)	LHSV (h ⁻¹)	SG 60/60	S (wt%)	N (wt ppm)	Di- aromatics (wt%)	Tri- aromatics (wt%)	PAH (wt%)
300	2	0.9369	0.1500	2058	7.7	20.1	27.8
300	4	0.9390	0.1588	2067	10.2	21.3	31.5
300	6	0.9406	0.1618	2080	9.9	21.4	31.6
350	2	0.9335	0.1049	1657	6.6	17.0	23.6
350	4	0.9365	0.1317	1870	9.2	18.1	27.3
350	6	0.9378	0.1442	1877	9.6	19.3	28.9

On page 15, lines 3-12:

A process for reducing content of sulphur compounds and polyaromatic hydrocarbons in a hydrocarbon feed having a boiling range between 200°C and 600°C is disclosed. The process comprises in combination contacting the feed and hydrogen over a hydrotreating catalyst and hydrotreating feed at hydrotreating conditions, cooling the hydrotreated effluent and hydrogen-rich gas from the hydrotreating reactor and contacting the effluent and hydrogen gas over a hydrotreating catalyst in a post-pretreatment reactor at a temperature sufficient to lower the polyaromatic hydrocarbon content.
